

# 基于均衡驱替的低渗透油藏直井压裂缝长优化方法

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**摘要:** 目前, 大多数油田采用相对规则的面积井网进行开发, 受储层非均质的影响, 各油田开发效果差异大。为此, 提出对位于渗透率低值区的采油井进行人工压裂的方法, 以达到井网均衡驱替的目的。以矩形五点井网为研究对象, 推导出矩形五点井网内压裂井与未压裂井的见水时间计算公式; 并以各采油井同时见水为目标, 结合流线积分法和等效井径法, 建立非均质油藏内位于渗透率低值区的压裂井的最优裂缝半长计算方法。通过分析储层渗透率级差、注采井距、注采压差差值及裂缝导流能力对压裂井最优裂缝半长的影响可知: 最优裂缝半长随注采压差差值和裂缝导流能力的增大而减小; 当储层渗透率级差和注采井距较大时, 压裂井所需的最优裂缝半长也较大。

**关键词:** 低渗透油藏 矩形五点井网 见水时间 裂缝半长 均衡驱替

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## Optimization method of fracture length of vertical wells in low-permeability reservoirs based on the equilibrium displacement

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**Abstract:** Relatively regular areal well pattern has been applied in most oilfields nowadays. But under the influence of reservoir heterogeneity, the development effect of different oilfields varies a lot. To solve this problem, a method of artificial fracturing for oil wells in low permeability zone was proposed, which aims to achieve the purpose of equilibrium displacement in well patterns. Targeting on the rectangular five-spot well pattern, the calculation formulas of water breakthrough time in the fractured oil well and the non-fractured oil well were derived. Besides, aiming at the target that the injected water reaches to different oil wells at the same time, a calculation method of the optimal fracture half-length of the fractured well in the low permeability zone of heterogeneous reservoir was established on the basis of stream line integral method and equivalent well diameter method. The influence of the permeability ratio, well spacing, the difference between two injection-production pressure differences and the fracture conductivity on the optimal fracture half-length was analyzed. The optimal fracture half-length decreases with the difference between two injection-production pressure differences and fracture conductivity. However, when the permeability ratio and the well spacing are large, the required optimal fracture half-length will be relatively long.

**Key words:** low-permeability reservoir; rectangular five-spot well pattern; water breakthrough time; fracture half-length; equilibrium displacement

21 世纪初, 李阳等针对非均质及各向异性油藏, 提出采用矢量井网的开发思想<sup>[1-2]</sup>。根据矢量井

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网设计的井网,各注采井距不再一致。这样的井网形式在开发初期能够达到较好的开发效果,但在后期进行井网加密调整或者井网形式调整时会造成较大困难,因此,目前油田在井网部署时仍采用相对规则的井网形式进行开发。然而,在非均质储层条件下,相对规则的井网形式容易导致驱替不均衡。对于低渗透油藏,人工压裂是改善储层渗透性、提高油井产量的有效方法<sup>[3]</sup>。于是,针对低渗透非均质油藏,提出对位于渗透率低值区的采油井进行人工压裂的方法,通过优化裂缝长度,使井网内部尽可能达到均衡驱替,从而改善井网的开发效果。

注采井网的均衡驱替是指各个注采井连线方向上的驱替程度相等<sup>[4]</sup>,即各采油井的见水时间相等。目前,已有不少学者对规则面积井网的产能计算方法<sup>[5]</sup>和压裂直井的产能计算方法<sup>[6-13]</sup>进行了研究。20世纪末至今,邓英尔等先后利用扰动椭圆思想、稳态依次替换思想、流管模型及流线积分法等,推导了面积井网的采油井见水时间计算公式<sup>[14-21]</sup>。但这些计算方法均未考虑规则面积井网中对采油井进行压裂的情况。为此,结合流线积分法和等效井径法,推导出矩形五点井网中压裂井的见水时间计算公式,并在此基础上,建立最优裂缝半长的计算方法,以期对低渗透非均质油藏面积井网优化开发调整措施提供理论依据。

## 1 五点井网的见水时间计算

### 1.1 未压裂井见水时间

一般来说,在考虑储层非均质性时,位于矩形五点井网内渗透率低值区的采油井会比其他3口采油井见水晚。因此,需对渗透率低值区的采油井进行人工压裂,将其见水时间适当提前。当压裂井与未压裂井的见水时间相等时,可视为该五点井网达到均衡驱替。为便于计算,将矩形五点井网看成4个一注一采单元的叠加(图1)。考虑储层非均质

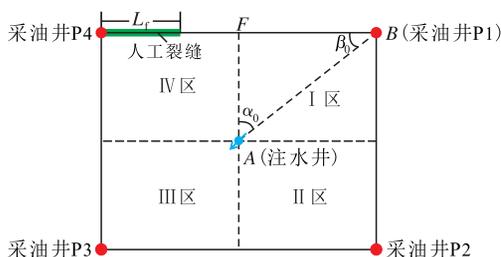


图1 压裂矩形五点井网单元示意

Fig.1 Sketch map of a fractured rectangular five-spot well pattern

性,设置每个一注一采单元内的储层参数相同,而各单元间储层参数各不相同;其中,采油井P4位于渗透率低值区(IV区),采油井P1,P2和P3位于渗透率高值区(I,II和III区),对采油井P4进行人工压裂。

针对图1中的渗透率高值区,在考虑对称性后,取其中任意一注一采单元的一半(如 $\triangle ABF$ ),作为一个计算单元。在计算单元 $\triangle ABF$ 中, $AF$ 为2个计算单元间的分流线,水驱油的流线不会与 $AF$ 相交,只会与之相切<sup>[19]</sup>。注入水从A点(注水井)出发,向B点(采油井P1)驱替,这个渗流过程可视为由无数个微元流管组合而成<sup>[22]</sup>。单根微元流管又可看作由无数流线组成,在流管内部,注入水仍沿流线向前驱替。为求得采油井的见水时间,先任取一微元流管,求得流管内水驱前缘到达采油井的时间;再令微元流管的中流线与计算单元的主流线重合,此时求出的流管内水驱前缘到达采油井的时间即可看作整个计算单元内采油井的见水时间。

在矩形五点井网计算单元 $\triangle ABF$ (图2)中,将四边形 $ADBC$ 看作一个微元流管,其中流线的长度等于 $L_1$ 和 $L_2$ 之和。微元流管从注水井和采油井出发的角度增量分别为 $\Delta\alpha$ 和 $\Delta\beta$ ,注水井和采油井的角变量( $\angle EAB$ 和 $\angle EBA$ )分别为 $\alpha$ 和 $\beta$ ,计算单元注水井和采油井处分流线与主流线的夹角( $\angle FAB$ 和 $\angle FBA$ )分别为 $\alpha_0$ 和 $\beta_0$ 。各角度之间的关系式<sup>[5]</sup>为

$$\frac{\beta}{\alpha} = \frac{\beta_0}{\alpha_0} = C_1 \quad (1)$$

则

$$\beta = C_1\alpha \quad (2)$$

$$\beta_0 = C_1\alpha_0 \quad (3)$$

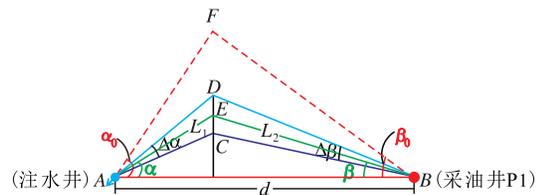


图2 矩形五点井网计算单元示意

Fig.2 Sketch map of the calculation unit in the rectangular five-spot well pattern

通过简化后的微元流管示意图(图3)可知,当水驱前缘沿微元流管中流线驱替至 $r$ 处时,该处对应的微元流管截面宽度和截面积分别为

$$l(r) = 2r \tan \frac{\Delta\alpha}{2} \quad (4)$$

$$A(r) = hl(r) \quad (5)$$

则从注水井和采油井出发的微元流管截面积可分

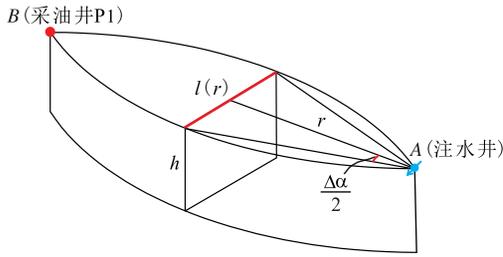


图3 微元流管示意

Fig.3 Sketch map of single micro flow tube

别近似为

$$\text{当 } r_{w1} \leq r_1 \leq L_1 = \frac{d \sin \beta}{\sin(\alpha + \beta)} \text{ 时, } A_1(r) = 2hr_1 \tan \frac{\Delta\alpha}{2} \quad (6)$$

$$\text{当 } 0 \leq r_2 \leq L_2 = \frac{d \sin \alpha}{\sin(\alpha + \beta)} - r_{w2} \text{ 时, } A_2(r) = 2hr_2 \tan \frac{\Delta\beta}{2} \quad (7)$$

对于油水两相非达西渗流,等饱和度面移动方程<sup>[23]</sup>为

$$\frac{dr}{dt} = \frac{v(t)}{\phi} f'_w(S_w) = \frac{q(t)}{\phi A(r)} f'_w(S_w) \quad (8)$$

注水开发时,当水驱前缘到达采油井井壁,即水驱前缘驱替过的距离为  $L$  时,可求得对应采油井的见水时间。因此,将式(8)沿  $L$  积分后可得

$$\int_{r_{w1}}^L A(r) dr = \int_0^T \frac{q(t) f'_w(S_{wf})}{\phi} dt \quad (9)$$

其中

$$L = \frac{d(\sin \alpha + \sin \beta)}{\sin(\alpha + \beta)} - r_{w2} \quad (10)$$

当注水量基本稳定时,  $q(t)$  可视为常数,即有

$$\int_0^T q(t) dt = q(t) T \quad (11)$$

将式(11)代入式(9),则式(9)可化简为

$$\int_{r_{w1}}^L A(r) dr = \frac{f'_w(S_{wf})}{\phi} q(t) T \quad (12)$$

对于低渗透油藏,需要考虑启动压力梯度<sup>[24-27]</sup>,当不考虑水相启动压力梯度的作用,仅考虑油相启动压力梯度的影响时<sup>[17]</sup>,微元流管截面流量的计算公式<sup>[20]</sup>为

$$q = \frac{CK}{\mu} A(r) \left( \frac{dp}{dr} - \lambda \right) \quad (13)$$

由于微元流管一般取得极小,此处微元流管截面流量可视为当  $\Delta\alpha \rightarrow 0$  对  $q$  求极限,则某时刻微元流管截面流量为

$$q(t) = \lim_{\Delta\alpha \rightarrow 0} q = \lim_{\Delta\alpha \rightarrow 0} \frac{CK}{\mu} A(r) \left( \frac{dp}{dr} - \lambda \right) = \lim_{\Delta\alpha \rightarrow 0} \frac{CK \left( \frac{dp}{dr} - \lambda \right)}{\frac{1}{A(r)}} \quad (14)$$

由于  $\Delta\alpha \rightarrow 0$ ,对式(14)运用洛必达法则,则式(14)变为

$$q(t) = \lim_{\Delta\alpha \rightarrow 0} \frac{\int_{r_{w1}}^L \frac{CK}{\mu} (dp - \lambda dr)}{\int_{r_{w1}}^L \frac{dr}{A(r)}} = \lim_{\Delta\alpha \rightarrow 0} \frac{CK \left( \Delta p - \lambda \int_{r_{w1}}^L dr \right)}{\int_{r_{w1}}^L \frac{dr}{A(r)}} \quad (15)$$

将式(6)、式(7)和式(10)代入式(15),进一步化简后可得

$$q(t) = \frac{2CKh}{\mu} \left\{ \Delta p - \lambda \left[ \frac{d(\sin \alpha + \sin \beta)}{\sin(\alpha + \beta)} - r_{w1} - r_{w2} \right] \right\} \frac{1}{\tan \frac{\Delta\alpha}{2} \ln \frac{d \sin \beta}{r_{w1} \sin(\alpha + \beta)} + \frac{1}{\tan \frac{\Delta\beta}{2} \ln \frac{d \sin \alpha}{r_{w2} \sin(\alpha + \beta)}} \quad (16)$$

将式(2)一式(7)及式(16)同时代入式(12),积分整理后可得

$$h \tan \frac{\Delta\alpha}{2} \left\{ \left[ \frac{d \sin(C_1\alpha)}{\sin(\alpha + C_1\alpha)} \right]^2 - r_{w1}^2 \right\} + h \tan \frac{\Delta\beta}{2} \left\{ \left[ \frac{d \sin \alpha}{\sin(\alpha + C_1\alpha)} \right]^2 - r_{w2}^2 \right\} = \frac{f'_w(S_{wf}) T}{\phi} \times \frac{2CKh}{\mu} \left\{ \Delta p - \lambda \left[ d \frac{\sin \alpha + \sin(C_1\alpha)}{\sin(\alpha + C_1\alpha)} - r_{w1} - r_{w2} \right] \right\} \frac{1}{\tan \frac{\Delta\alpha}{2} \ln \frac{d \sin(C_1\alpha)}{r_{w1} \sin(\alpha + C_1\alpha)} + \frac{1}{\tan \frac{\Delta\beta}{2} \ln \frac{d \sin \alpha}{r_{w2} \sin(\alpha + C_1\alpha)}} \quad (17)$$

考虑到流体在地层渗流过程中存在“舌进现象”,注入水会沿主流线率先突进到采油井。也就是说,当角变量  $\alpha$  和  $\beta$  均趋近于0时,对式(17)求极限,即可求得采油井的见水时间。当  $\alpha \rightarrow 0$  且  $\beta \rightarrow 0$  时,微元流管中流线与主流线重合,且微元流管关于注采井连线  $AB$  的垂直平分线呈轴对称,此时,  $\Delta\beta = \Delta\alpha$ , 则  $\tan \frac{\Delta\beta}{2} = \tan \frac{\Delta\alpha}{2}$ 。当  $\alpha \rightarrow 0$  时,由洛必达法则,有

$$\lim_{\alpha \rightarrow 0} \frac{\sin(C_1\alpha)}{\sin(\alpha + C_1\alpha)} = \frac{C_1}{1 + C_1} \quad (18)$$

$$\lim_{\alpha \rightarrow 0} \frac{\sin \alpha}{\sin(\alpha + C_1\alpha)} = \frac{1}{1 + C_1} \quad (19)$$

$$\lim_{\alpha \rightarrow 0} \frac{\sin \alpha + \sin C_1\alpha}{\sin(\alpha + C_1\alpha)} = 1 \quad (20)$$

将式(18)一式(20)代入式(17),化简可得

$$\frac{d^2(1+C_1^2)}{(1+C_1)^2} - r_{w1}^2 - r_{w2}^2 = \frac{f'_w(S_{wf})T}{\phi} \times \frac{2CK}{\mu} \times \frac{\Delta p - \lambda(d-r_{w1}-r_{w2})}{2 \ln \frac{d}{1+C_1} + \ln \frac{C_1}{r_{w1}r_{w2}}} \quad (21)$$

将式(21)整理后可得计算单元内未压裂井的见水时间表达式为

$$T = \frac{\phi \mu \left[ \frac{d^2(1+C_1^2)}{(1+C_1)^2} - r_{w1}^2 - r_{w2}^2 \right] \left( 2 \ln \frac{d}{1+C_1} + \ln \frac{C_1}{r_{w1}r_{w2}} \right)}{2CKf'_w(S_{wf})[\Delta p - \lambda(d-r_{w1}-r_{w2})]} \quad (22)$$

## 1.2 压裂井见水时间

对于有限导流垂直裂缝井,可基于其与普通直井产量相等的原理,推导出该井的等效井径。王晓东等给出了有限导流垂直裂缝井的产量公式,并根据Prats方法,推导得到有限导流垂直裂缝井的等效井径表达式<sup>[28-29]</sup>为

$$r_{we} = 2L_f e^{-\left[\frac{3}{2} + f(C_{th}) + S_i\right]} \quad (23)$$

其中

$$f(C_{th}) = \frac{1.65 - 0.328u + 0.116u^2}{1.0 + 0.18u + 0.064u^2 + 0.005u^3} \quad (24)$$

$$u = \ln C_{th} \quad (25)$$

$$C_{th} = \frac{K_f w_f}{KL_f} \quad (26)$$

$$S_i = \frac{\pi w_f}{2L_f} \left( \frac{K}{K_f} - 1 \right) \quad (27)$$

将位于IV区的压裂直井等效成为1口普通直井,其等效井径为 $r_{we}$ 。若忽略不计流体在裂缝内的流动时间,则利用流线积分法推导出的未压裂井见水时间公式可直接用于计算压裂井的见水时间,需要注意的是,式(22)中的 $r_{w2}$ 需用等效井径 $r_{we}$ 代替,则计算单元内压裂井的见水时间表达式为

$$T_i = \frac{\phi \mu \left[ \frac{d^2(1+C_1^2)}{(1+C_1)^2} - r_{w1}^2 - r_{we}^2 \right] \left( 2 \ln \frac{d}{1+C_1} + \ln \frac{C_1}{r_{w1}r_{we}} \right)}{2CK_h f'_{wh}(S_{wf})[\Delta p_h - \lambda_h(d-r_{w1}-r_{we})]} \quad (28)$$

当矩形五点井网达到均衡驱替,未压裂井与压裂井的见水时间相等,由此计算出压裂井的等效井径,再根据式(23)计算压裂井的裂缝半长。

## 2 最优裂缝半长计算及准确性验证

建立低渗透油藏平面非均质正方形反五点井

网模型,注水井位于井网中心,生产井位于四角。储层参数包括:油层厚度为20 m,油层顶界深度为3 000 m,储层孔隙度为0.15;储层渗透率具平面非均质性,采油井P4位于渗透率低值区(IV区),该区渗透率为3 mD;其他3口采油井位于渗透率高值区(I、II和III区),且渗透率初值相等,均为9 mD;渗透率高值区内的含水率对水驱前缘含水饱和度的导数比渗透率低值区内的略小;储层渗透率级差为3。对应不同储层渗透率,启动压力梯度随渗透率的减小而增大<sup>[30]</sup>,设置渗透率低值区的启动压力梯度为0.036 7 MPa/m,渗透率高值区的启动压力梯度为0.035 6 MPa/m。对采油井P4进行压裂,裂缝宽度为0.02 m,裂缝渗透率为60 000 mD。地层原油密度850 kg/m<sup>3</sup>,地层水密度为1 000 kg/m<sup>3</sup>;地层原油粘度为2 mPa·s,地层水粘度为0.4 mPa·s。注采井排距与采油井井距的一半相等,为150 m,注采井距为212 m,采油井和注水井的井径均为0.1 m,注采压差为20 MPa。对于所建模型, $C_1 = 1$ 。

当压裂井与未压裂井的见水时间相等时,认为井网内达到均衡驱替。令 $T = T_i$ ,即式(22)与式(28)相等,化简后可得

$$\frac{\left[ \frac{d^2(1+C_1^2)}{(1+C_1)^2} - r_{w1}^2 - r_{w2}^2 \right] \left( 2 \ln \frac{d}{1+C_1} + \ln \frac{C_1}{r_{w1}r_{w2}} \right)}{Kf'_w(S_{wf})[\Delta p - \lambda(d-r_{w1}-r_{w2})]} = \frac{\left[ \frac{d^2(1+C_1^2)}{(1+C_1)^2} - r_{w1}^2 - r_{we}^2 \right] \left( 2 \ln \frac{d}{1+C_1} + \ln \frac{C_1}{r_{w1}r_{we}} \right)}{K_h f'_{wh}(S_{wf})[\Delta p_h - \lambda_h(d-r_{w1}-r_{we})]} \quad (29)$$

由于式(29)为关于 $r_{we}$ 的超越方程,无法求得 $r_{we}$ 的精确表达式。为此,采用牛顿迭代法,计算得到压裂井的等效井径为18.85 m,再由式(23)计算得到压裂井的裂缝半长为126 m。笔者将利用该方法计算得到的裂缝半长称为达到均衡驱替时压裂井的最优裂缝半长。

根据计算结果,采用油藏数值模拟软件,对推导得到的见水时间及最优裂缝半长计算方法进行验证。针对上述低渗透油藏平面非均质反五点井网模型,建立油藏数值模拟模型进行模拟计算。各采油井在采油井P4压裂前、后的见水时间对比结果(图4)表明:采用新建方法计算得到的最优裂缝半长进行压裂后,采油井P4的见水时间大幅提前;且压裂后,该正方形五点井网内4口采油井的见水时间相差很小,井网基本达到均衡驱替。说明所建见水时间和最优裂缝半长计算方法是正确、可行的。

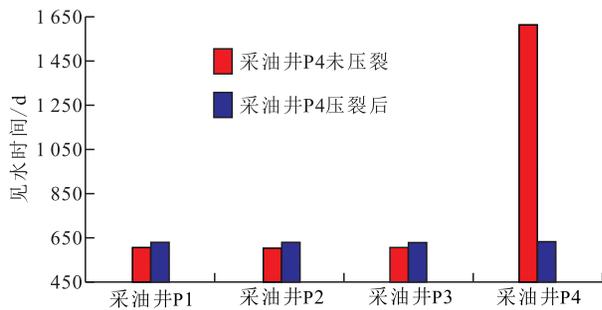


图4 油藏数值模拟计算的各采油井见水时间

Fig.4 Comparison of the water breakthrough time of different oil wells calculated by reservoir numerical simulation

### 3 最优裂缝半长影响因素

对于不同物性及非均质性的储层,渗透率低值区的压裂井所需的最优裂缝半长不同。在储层渗透率级差为3、采油井井距为300 m、裂缝渗透率为50 000 mD和缝宽为0.01 m的条件下,模拟计算不同注采压差下对应的压裂井最优裂缝半长。

将注水井与采油井P4间的注采压差和注水井与采油井P1间的注采压差的差值定义为注采压差差值,绘制最优裂缝半长与注采压差差值的关系曲线。由图5可以看出,压裂井的最优裂缝半长随注采压差差值的增大而减小。当注采压差差值为1~3 MPa时,最优裂缝半长随注采压差差值的增大而骤减;当注采压差差值为3~5 MPa时,递减趋势逐渐变缓。当注采压差差值大于3 MPa时,压裂井的最优裂缝半长仅为3~17 m。因此,在注水井与压裂井间的注采压差和注水井与未压裂井间的注采压差相差不大时,可以通过优化压裂井的裂缝缝长达到均衡驱替;当注采压差能够大幅提升时,可不进行压裂,通过提高注采压差的方式达到井网均衡驱替的目的。

在储层渗透率级差为3、采油井井距为300 m和

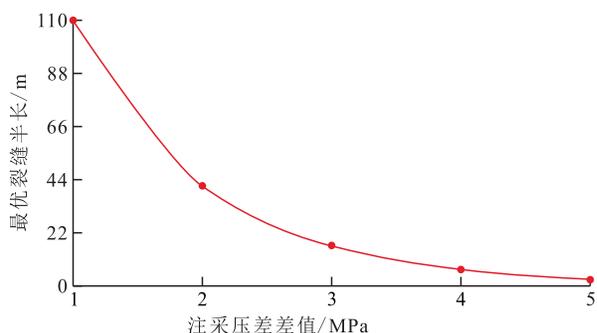


图5 最优裂缝半长与注采压差差值的关系

Fig.5 Relationship between the optimal fracture half-length and the difference between two injection-production pressure differences

注采压差为20 MPa的条件下,压裂井的最优裂缝半长随裂缝导流能力的增大而减小(图6)。当裂缝导流能力小于140 D·cm时,裂缝导流能力每增大20 D·cm,最优裂缝半长会相应减小10~15m。当裂缝导流能力大于140 D·cm时,最优裂缝半长递减趋势逐渐变缓;裂缝导流能力每增大20 D·cm,最优裂缝半长仅减小约2~5 m。

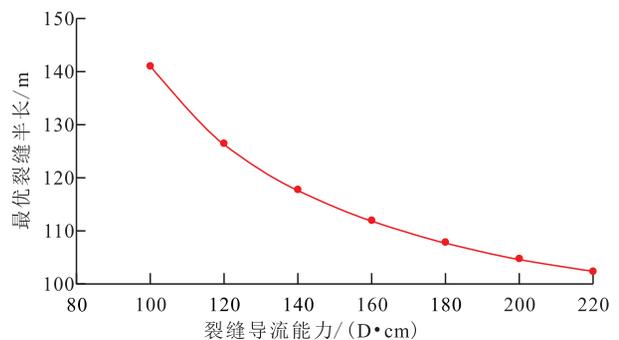


图6 最优裂缝半长与裂缝导流能力的关系

Fig.6 Relationship between the optimal fracture half-length and the fracture conductivity

为分析储层非均质性对最优裂缝半长的影响,设置裂缝渗透率为10 0000 mD,缝宽为0.02 m、注采压差为20 MPa、采油井井距和储层渗透率级差不同、且各个级差下储层平均渗透率相同,计算不同采油井井距和不同渗透率级差下的最优裂缝半长,绘制不同井距对应的最优裂缝半长与渗透率级差的关系曲线。结果(图7)表明:压裂井的最优裂缝半长随渗透率级差的增大而增大;在同一渗透率级差下,采油井井距越大,需要的最优裂缝半长越大。

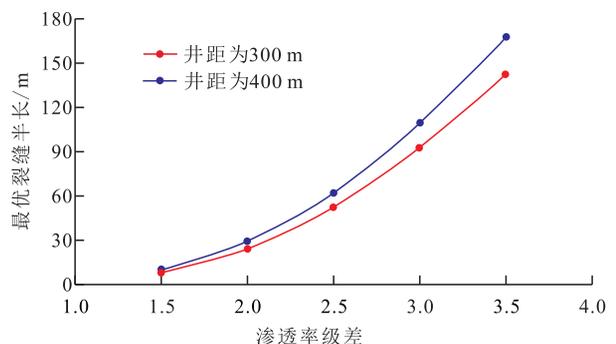


图7 最优裂缝半长与渗透率级差的关系

Fig.7 Relationship between the optimal fracture half-length and the permeability ratio

### 4 结论

运用流线积分法和等效井径法,推导出低渗透油藏压裂井及未压裂井的见水时间计算公式。

在平面非均质低渗透储层井网中,对位于渗透率低值区的采油井进行人工压裂,可以有效改善井

网内的平面非均质性,提高井网均衡驱替程度。基于各采油井见水时间相等的原则,结合流线积分法和等效井径法,推导出均衡驱替情况下渗透率低值区压裂井的最优裂缝半长计算方法。

储层渗透率级差、启动压力梯度、注采井距、注采压差及裂缝导流能力均会对压裂井的最优裂缝半长产生较大影响。

#### 符号解释:

$\alpha_0$ ——注水井处分流线与主流线的夹角, ( $^\circ$ );  $\beta_0$ ——采油井处分流线与主流线的夹角, ( $^\circ$ );  $L_f$ ——压裂井的裂缝半长, m;  $\alpha$ ——注水井的角变量, ( $^\circ$ );  $\beta$ ——采油井的角变量, ( $^\circ$ );  $\Delta\alpha$ ——注水井处的角度增量, ( $^\circ$ );  $\Delta\beta$ ——采油井处的角度增量, ( $^\circ$ );  $d$ ——注采井距, m;  $L_1$ ——微元流管中流线从注水井中心到拐点  $E$  的长度, m;  $L_2$ ——微元流管中流线从拐点  $E$  到采油井井壁的长度, m;  $l(r)$ ——微元流管  $r$  处的截面宽度, m;  $r$ ——水驱前缘驱替过的距离, m;  $A(r)$ ——微元流管  $r$  处的截面积,  $m^2$ ;  $h$ ——储层厚度, m;  $r_{w1}$ ——注水井井径, m;  $r_1$ ——水驱前缘从注水井中心出发驱替过的距离, m;  $A_1(r)$ ——微元流管  $r_1$  处的截面积,  $m^2$ ;  $r_2$ ——水驱前缘从拐点  $E$  出发驱替过的距离, m;  $r_{w2}$ ——采油井井径, m;  $A_2(r)$ ——微元流管  $r_2$  处的截面积,  $m^2$ ;  $t$ ——水驱前缘驱替至  $r$  时所对应的时间, s;  $v$ ——流体渗流速度, m/s;  $\phi$ ——储层孔隙度;  $f_w$ ——渗透率高值区的含水率;  $S_w$ ——含水饱和度;  $q$ ——微元流管的截面流量,  $m^3/d$ ;  $L$ ——微元流管中流线从注水井中心到采油井井壁的长度, m;  $T$ ——未压裂井的见水时间, s;  $S_{wf}$ ——水驱前缘含水饱和度;  $C$ ——单位换算系数, 其值为 0.086 4;  $K$ ——渗透率高值区的渗透率, mD;  $\mu$ ——地层流体粘度,  $mPa \cdot s$ ;  $p$ ——地层压力, MPa;  $\lambda$ ——渗透率高值区的启动压力梯度, MPa/m;  $\Delta p$ ——渗透率高值区的注采压差, MPa;  $r_{we}$ ——等效井径, m;  $K_f$ ——裂缝渗透率, mD;  $w_f$ ——裂缝宽度, m;  $T_f$ ——压裂井的见水时间, s;  $K_h$ ——渗透率低值区的渗透率, mD;  $f_{wh}$ ——渗透率低值区的含水率;  $\Delta p_h$ ——渗透率低值区的注采压差, MPa;  $\lambda_h$ ——渗透率低值区的启动压力梯度, MPa/m。

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