

文章编号:1009-9603(2020)01-0036-09

DOI:10.13673/j.cnki.cn37-1359/te.2020.01.005

# 不同油藏压力下CO<sub>2</sub>驱最小混相压力实验研究

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**摘要:**CO<sub>2</sub>-原油体系的最小混相压力是影响CO<sub>2</sub>驱开发效果的关键因素。随油藏开发阶段的不断深入,当油藏压力低于原始饱和压力后,溶解在原油中的溶解气会部分脱出。油藏流体组分及其高压物性也会发生变化,影响CO<sub>2</sub>-原油体系的最小混相压力,利用原始地层流体样品测试得到的最小混相压力不再适用。为此,以中国西部某油田8个典型区块为例,进行细管实验测试和多组分数值模拟,对不同油藏压力下的最小混相压力进行系统研究。与其他油田相比,研究区各油藏油样的C<sub>1</sub>摩尔含量较高,为31.12%~51.69%,平均为43.25%;C<sub>2</sub>-C<sub>6</sub>摩尔含量较低,为8.0%~18.48%,平均仅为11.3%。细管实验和数值模拟结果表明,在原始地层压力下,CO<sub>2</sub>均与8个典型区块地层原油样品发生混相驱替,但不同区块CO<sub>2</sub>驱最小混相压力差异很大,其值为17.60~41.18 MPa。当油藏压力低于原始饱和压力后,CO<sub>2</sub>驱最小混相压力主要呈微小幅度下降的趋势。随脱气压力进一步降低,油相组分构成中,C<sub>1</sub>N<sub>2</sub>摩尔含量呈递减趋势,C<sub>7</sub><sup>+</sup>和C<sub>24</sub><sup>+</sup>组分呈递增趋势,而中间组分(C<sub>2</sub>和C<sub>3</sub><sup>+</sup>)摩尔含量变化较小。在各级脱气压力下,脱出气体以C<sub>1</sub>为主,中间组分摩尔含量仅在最后一级脱气压力下急剧升高。CO<sub>2</sub>-原油混相带出现在注入CO<sub>2</sub>波及前缘靠近注入端的位置,混相带随着驱替的进行而逐渐变宽。

**关键词:**CO<sub>2</sub>驱;最小混相压力;饱和压力;溶解气;组分变化

中图分类号:TE357.45

文献标识码:A

## Study on minimum miscibility pressure of CO<sub>2</sub> flooding at different reservoir pressures

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**Abstract:** The minimum miscibility pressure (MMP) of the CO<sub>2</sub>-crude oil system is a key factor affecting the development effect of CO<sub>2</sub> flooding. When the reservoir pressure is lower than the original saturation pressure, the part solution gas dissolved in the oil will be separated from the oil with the development of oil reservoir. Thus, the composition of oil phase and its high-pressure physical properties will also change, which will affect the MMP of CO<sub>2</sub>-crude oil system. The MMP obtained from the original formation oil sample is no longer applicable. Based on the slim tube experiment and multi-component numerical simulation, the MMPs of crude oil samples at different reservoir pressures in eight typical blocks of an oilfield in western China are systematically studied. Compared with other oilfields in China, the C<sub>1</sub> molar content of oil samples from various reservoirs in the study area is higher, ranging from 31.12% to 51.69%, with an average of 43.25%; while the molar content of C<sub>2</sub>-C<sub>6</sub> is lower, ranging from 8.0% to 18.48%, with an average of only 11.3%. The experimental and simulation results show that CO<sub>2</sub> can be miscible with the oil samples from eight typical blocks under at original reservoir

收稿日期:2019-08-21。

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基金项目:国家科技重大专项“低渗-致密储层不同提高采收率方法下油藏工程评价”(2017ZX05009004-005),国家自然科学基金石油化工联合基金项目“超低渗透油藏渗流规律与高效开发的关键科学问题”(U1762210)。

pressures, but the MMPs of CO<sub>2</sub> flooding in various blocks have significant differences, ranging from 17.60 MPa to 41.18 MPa. After the reservoir pressure is lower than the original saturation pressure, the MMPs in CO<sub>2</sub> flooding of typical reservoir oil samples tend to decrease slightly. With further decrease of degassed pressure, the molar content of C<sub>1</sub>N<sub>2</sub> in the oil phase decreases, the molar contents of C<sub>7</sub><sup>+</sup> and C<sub>24</sub><sup>+</sup> increase, and the changes of C<sub>2</sub> and C<sub>3</sub><sup>+</sup> are minor. C<sub>1</sub> is the main component of the separated gas at different pressures. The intermediate component increases sharply only at the last degassing pressure. CO<sub>2</sub>-crude oil miscible zone occurs at the swept front of the injected CO<sub>2</sub> close to the injection side. The miscible zone becomes wider with the displacement.

**Key words:** CO<sub>2</sub> flooding; minimum miscibility pressure; saturation pressure; solution gas; composition variation

CO<sub>2</sub>驱是一项久经验证的提高石油采收率技术。近年来,随着全球气候变暖,如何减少CO<sub>2</sub>等温室气体的排放并实现资源化利用备受关注<sup>[1-5]</sup>。CO<sub>2</sub>驱不仅可以提高石油采收率,还能封存注入油藏的CO<sub>2</sub>,从而实现温室气体减排并带来可观的环保效益<sup>[6-8]</sup>。在高温高压状态下,CO<sub>2</sub>在油藏中通常处于超临界状态,既具有与气体相当的高扩散系数和低黏度,又具有与液体相近的密度和良好的溶解能力,低黏度、高扩散性的特点利于溶解在其中的物质扩散和向固体基质的渗透。当CO<sub>2</sub>与原油发生作用后,可有效降低原油黏度,膨胀原油体积,改善流度比,从而与原油发生混相作用,提高石油采收率。研究表明,CO<sub>2</sub>驱可将采收率提高8%~15%,开采期延长约12~20 a<sup>[9-17]</sup>。落实油田CO<sub>2</sub>驱可行性研究的第一步是进行筛选,对CO<sub>2</sub>注入效果和性能进行合理评估。符合筛选条件的油田需要进一步开展细管实验以评估CO<sub>2</sub>驱最小混相压力(MMP)。

细管实验是行业通用的获得驱替流体和原油之间MMP的标准方法。除升泡法、界面张力消失法等实验外,MMP还可以通过经验公式法<sup>[18-22]</sup>、状态方程法<sup>[23-24]</sup>、系数法<sup>[25-27]</sup>和混合单元网格法<sup>[28-32]</sup>等方法获得。虽然相关文献给出的MMP预测值与实验值之间具有较高的吻合度,但对其可靠性仍然存在疑虑<sup>[33]</sup>。原油和CO<sub>2</sub>间的混溶性主要受油藏温度、压力和原油性质等因素影响<sup>[34-37]</sup>。若注入CO<sub>2</sub>中含有CH<sub>4</sub>或N<sub>2</sub>等杂质气体会增加MMP,而H<sub>2</sub>S、C<sub>2</sub>和C<sub>3</sub>等气体增加会显著降低MMP<sup>[38-41]</sup>。YELLIG等研究发现,对于饱和油藏即使油藏温度恒定,气油比在不同区域的变化也会导致CO<sub>2</sub>驱MMP变化<sup>[42]</sup>。尽管已经认识到地层原油组分和注入流体对MMP具有较大影响,但原油中溶解气是如何影响MMP的专门研究鲜有报道。油藏发生脱气后,特定油样MMP的研究更是少之又少<sup>[43-44]</sup>。当油藏压力低至原始饱和压力后,溶解在原油中的溶解气会部分脱出,此时根据原始地层流体测试获得的MMP是不准确的。

为此,根据储层物性和原油性质等从中国西部

某油田筛选出8个典型区块作为研究对象,编号依次为S1—S8,结合高压物性分析、细管实验、多相多组分数值模拟,研究不同油藏压力下的MMP变化规律,以期为该油田CO<sub>2</sub>提高采收率机理和CO<sub>2</sub>混相驱应用潜力提供理论依据,为持续推广CO<sub>2</sub>混相驱技术,保持目标油田持续稳产及CO<sub>2</sub>混相驱技术整体布局提供技术支撑。

## 1 实验器材与方法

### 1.1 实验器材

实验器材主要包括地层流体配样仪、PVT分析仪和HA-IV型油气藏动态监测反演系统装置。HA-IV型油气藏动态监测反演系统装置包括Teledyne ISCO100DX型恒压恒速泵、中间容器、细管模型、高温高压观察窗、回压调节器、油气分离器、数据采集系统、气量计、高压管线及阀门若干。

细管模型为内部均匀充填一定粒径范围且经压实的石英砂的不锈钢细管,长度均为20.0 m,渗透率为3 850~4 100 mD。实验所用的CO<sub>2</sub>气体由北京永圣气体技术有限公司提供,纯度为99.95%。细管实验装置流程如图1所示。

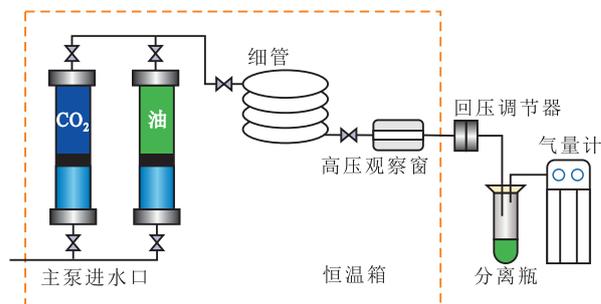


图1 细管实验流程

Fig.1 Flow chart of slim tube experiment

### 1.2 实验方法

#### 1.2.1 地层流体配制

原油样品为井口取样,按照各样品产出气组成配置标准气与相应原油进行复配获得地层油样品,经检验样品均合格,各样品井流物组分全烃分析结

果如图2所示。

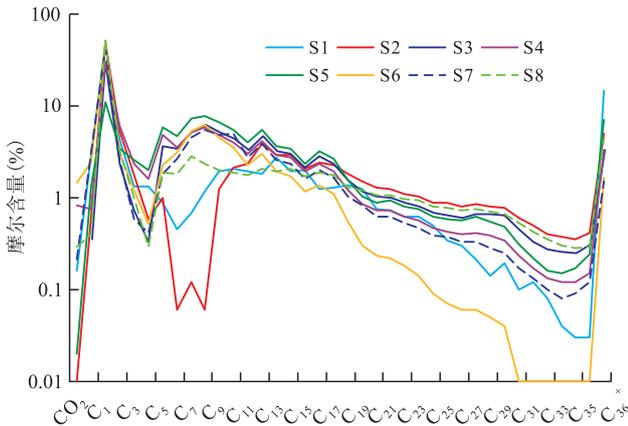


图2 8个典型区块各样品井流物组分构成

Fig.2 Composition of well effluents of oil samples from eight typical blocks

全烃分析结果表明,各地层油样品中CH<sub>4</sub>摩尔含量为31.12%~51.69%,平均为43.25%,高于其他油田;而中间组分平均摩尔含量仅为11.3%,在所调研的油田中处于较低水平(图3)。

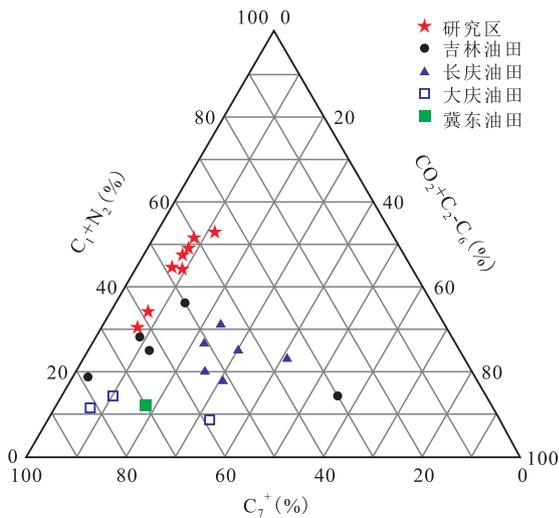


图3 典型油田原油三元拟组分

Fig.3 Ternary pseudo-component of oil samples from typical oilfields

### 1.2.2 高压物性测试

采用法国ST公司生产的无汞全透明活塞式高压PVT分析仪,对所配置的地层油样品进行高压物性实验,该设备可实现在高温高压(200℃,150MPa)下测试、可视、实时地记录实验过程并自动采集测试数据(表1)。

通过单次脱气、恒质膨胀、多次脱气和黏度测试等实验获得各典型区块油藏样品在高温高压下的物性参数,并使用Eclipse软件校正拟组分临界参数和状态方程参数,为获得连续性的状态方程参数提供实验依据。通过多次脱气实验获得闪蒸油样品,以代表不同压力下脱出部分溶解气的地层原

表1 8个典型区块油藏基本物性参数及MMP测试结果

Table1 Basic physical parameters and MMP test results from eight typical reservoirs

样品编号	地层温度(℃)	原始地层压力(MPa)	原始饱和压力(MPa)	目前地层压力(MPa)	气油比(m <sup>3</sup> /m <sup>3</sup> )	MMP(MPa)
S1	72.0	35.66	30.35	22.79	179	34.37
S2	75.0	37.50	27.50	24.72	133	36.42
S3	62.0	25.50	12.20	20.21	65	18.86
S4	60.0	20.80	14.40	18.40	76	28.06
S5	89.0	59.30	6.10	36.75	31	17.60
S6	74.8	33.10	26.40	40.20	188	26.40
S7	90.0	62.50	23.63	56.00	180	33.10
S8	103.8	38.45	38.45	33.46	131	41.18

油,即具有不同饱和和压力的地层原油。

### 1.3 不同油藏压力下CO<sub>2</sub>驱最小混相压力实验

在一定温度条件下,给定地层原油和CO<sub>2</sub>间形成混相所需的最低压力即为CO<sub>2</sub>驱MMP。CO<sub>2</sub>驱细管实验均在各样品地层温度下开展,每个地层油样品共设置6组不同驱替压力,当注入CO<sub>2</sub>量达到1.2PV时,停止实验,并绘制驱替压力与驱油效率的关系曲线(图4),根据曲线的拐点来确定MMP。细管实验测得的各典型区块原始地层油CO<sub>2</sub>驱MMP如表1所示。

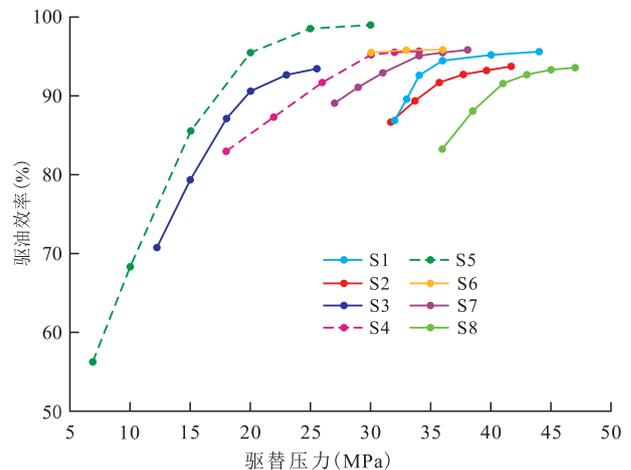


图4 各地层油样品CO<sub>2</sub>驱的驱替压力与驱油效率关系

Fig.4 Relationship between displacement pressure and displacement efficiency of oil samples from various formations during CO<sub>2</sub> flooding

### 1.4 不同油藏压力下CO<sub>2</sub>驱最小混相压力评价实验

通过高压物性分析开展的多次脱气实验,可以获得不同油藏压力(各级脱气压力)下的地层原油样品和脱出气体。由于在多次脱气实验过程中,有一定量的溶解气从原始地层油中脱出,导致剩余地

层原油的组分构成比例发生变化,这一过程与开发过程中油藏压力的下降导致溶解气析出并使油相(气油比小于原始气油比)的组分构成比例发生变化一致。将不同脱气压力下剩余地层油用来模拟不同油藏压力下的地层油样品。

考虑到细管实验的耗时性,仅对S7样品开展不同油藏压力下油藏流体组分发生变化后的CO<sub>2</sub>驱细管实验,用以验证数值模拟研究的可靠性。S7样品实验温度为90℃,原始饱和压力为23.63 MPa,通过多次脱气实验,获得20, 15和10 MPa下油相流体样品,分别用于细管实验,测试相应的MMP(图5)。当油藏压力依次降低至20, 15和10 MPa时,油藏压力下降造成的溶解气脱出使相同驱替压力下脱气油的采出程度高于原始地层油。相应的MMP从33.10 MPa下降至31.86 MPa。

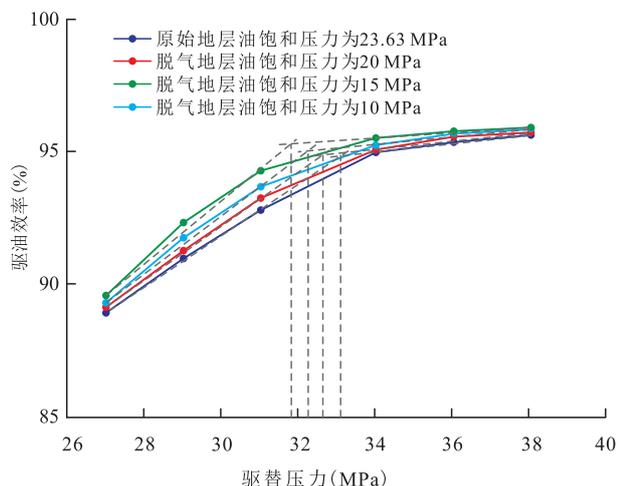


图5 S7和脱气S7样品的驱替压力与驱油效率关系曲线  
Fig.5 Relationship between displacement pressure and displacement efficiency of S7 and degassed S7 samples

## 2 数值模拟研究及讨论

### 2.1 数值模拟模型的建立

数值模拟方法是混相驱效果评价和混相驱设计的重要方法。在高压物性实验的基础上,建立考虑多组分的一维数值模拟模型对细管实验进行仿真。将细管模型理想化为一维网格且仅沿水平方向等分,截面为0.386 cm×0.386 cm的正方形,其他模型参数与实际细管模型相同。在第1个网格内设置1个注入量恒定的注入井,在最后1个网格内设置1个压力恒定的生产井。在储层条件下进行细管实验的数值模拟研究。

### 2.2 不同油藏压力下最小混相压力变化规律

各样品的数值模拟值与细管实验值相对误差

为0.29%~1.92%,拟合效果较好(图6)。将原始地层油样品的数值模拟模型对细管实验值历史拟合达到要求后,再开展不同油藏压力下的MMP数值模拟研究。结果表明,S7样品在不同油藏压力下的数值模拟MMP与实验测得的MMP平均相对误差仅为0.43%,数值模拟预测效果与实验研究一致。

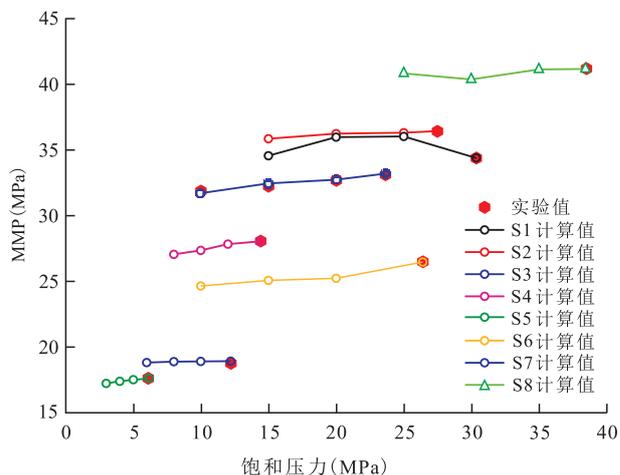


图6 不同饱和压力下各地层油样品的MMP变化规律  
Fig.6 MMP variation of oil samples from various formations at different saturation pressures

数值模拟结果表明,当油藏压力低于原始饱和压力后,在饱和压力随着油藏压力下降而不断减小的过程中,MMP主要呈缓慢降低的趋势,整体下降幅度较小;仅S1样品MMP先上升后下降。研究区地层油组分中溶解气主要以C<sub>1</sub>为主,当油藏压力低于原始饱和压力后,溶解气脱出是MMP降低的原因之一。

### 2.3 不同油藏压力下地层油组分变化规律

不同油藏压力下地层油拟组分变化规律如图7所示,当油藏压力从原始饱和压力( $p_b$ )依次降至一级饱和压力( $p_1$ )、二级饱和压力( $p_2$ )和三级饱和压力( $p_3$ )时,各样品均呈轻组分摩尔含量减少、重组分摩尔含量增加的变化趋势。

各拟组分变化规律表明,C<sub>1</sub>N<sub>2</sub>呈大幅递减趋势;C<sub>7</sub><sup>+</sup>和C<sub>24</sub><sup>+</sup>呈递增趋势;而C<sub>2</sub>和C<sub>3</sub><sup>+</sup>变化较小。混相驱研究表明CH<sub>4</sub>含量的减少将会使MMP降低,而重组分,如C<sub>24</sub><sup>+</sup>摩尔含量的增加,使MMP增加,若CH<sub>4</sub>摩尔含量降低的影响大于重组分摩尔含量增加的影响,最终使研究区不同油藏压力下的地层油样品CO<sub>2</sub>驱MMP主要呈小幅度下降的趋势,有待开展进一步的针对性研究。

### 2.4 不同油藏压力下脱出气组分变化规律

分析脱出气组分色谱(图8)表明,当油藏压力从 $p_b$ 依次降至 $p_1$ , $p_2$ , $p_3$ 和四级饱和压力( $p_4$ )时,脱出气组分以CH<sub>4</sub>为主,中间组分摩尔含量低于其在产

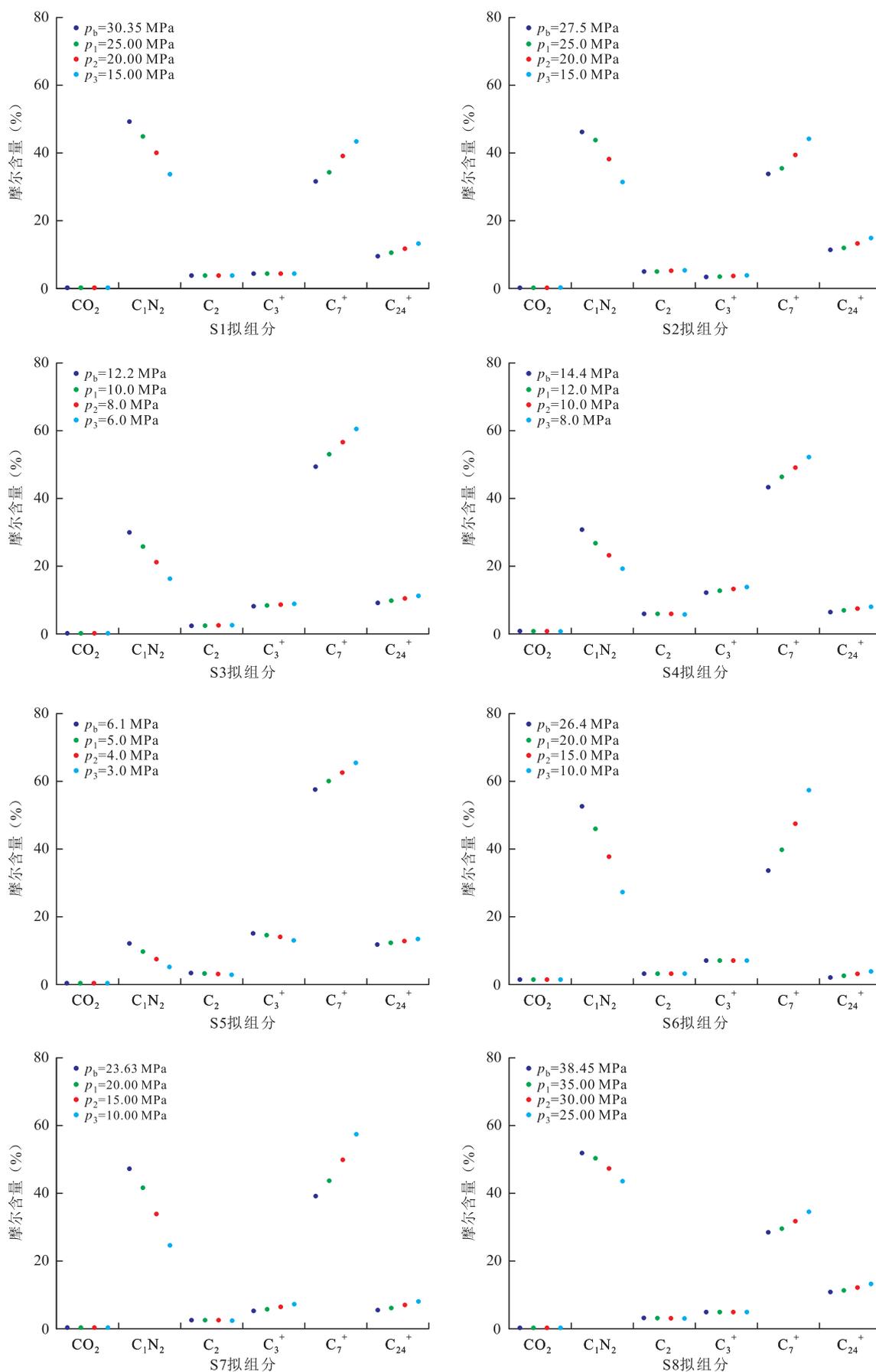


图7 不同油藏压力下地层油拟组分变化规律

Fig.7 Pseudo-composition variation of formation oil at different reservoir pressures

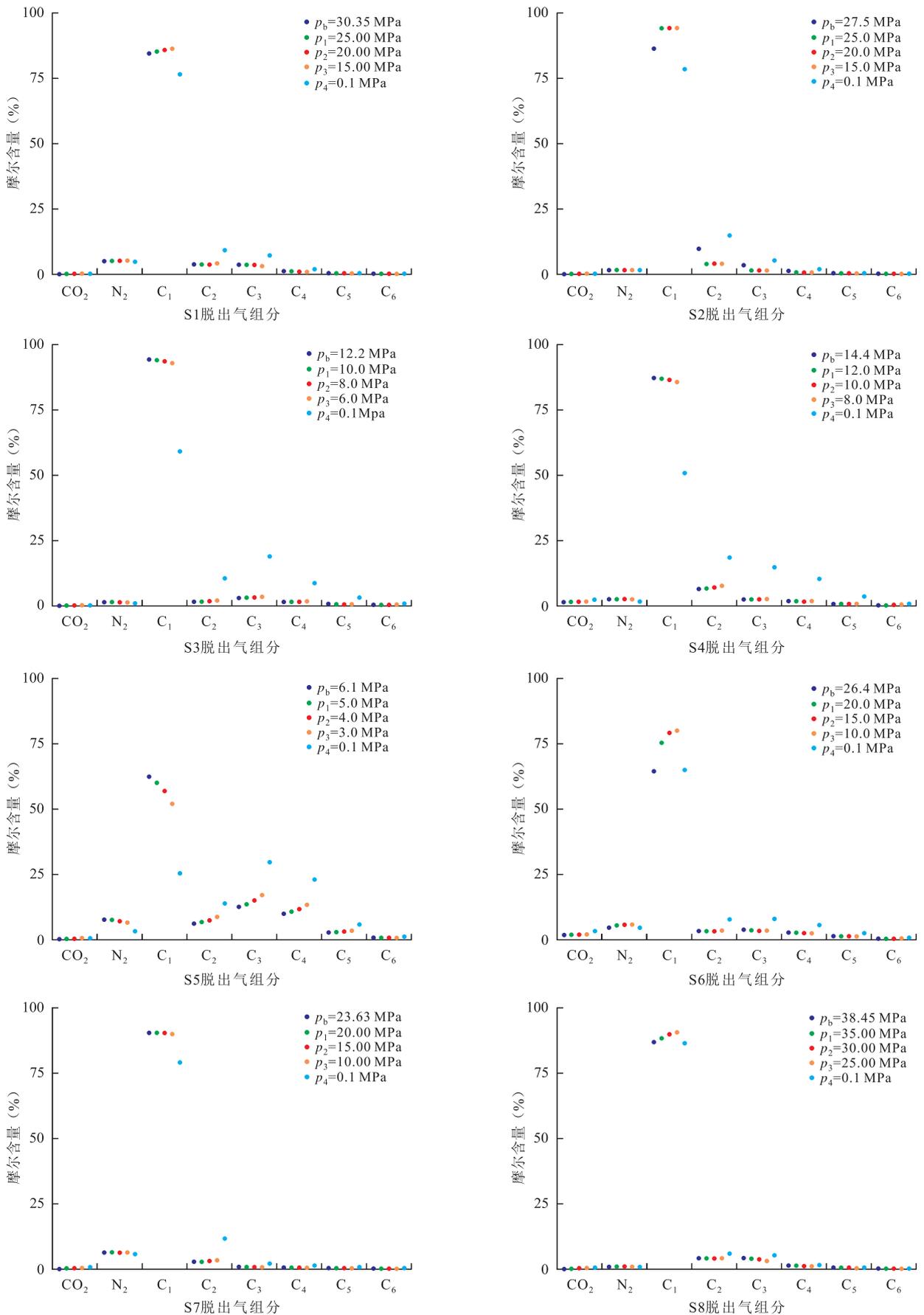


图8 不同油藏压力下脱出气组分变化规律

Fig.8 Degassing composition variation at different reservoir pressures

出气中的占比。只有当油藏压力降至0.1 MPa时,中间组分烃类才会大量脱出,并远高于其在产出气中的占比。

### 2.5 CO<sub>2</sub>-原油混相带特征

CO<sub>2</sub>驱细管实验数值模拟不仅可以通过采出程度与压力的关系曲线确定MMP,还可以通过Flviz模块可视化界面观察CO<sub>2</sub>驱细管模拟过程中界面张力的变化,并可以进一步分析CO<sub>2</sub>驱混相带的发展和演变特征。在数值模拟中,可以根据油气的摩尔密度、摩尔分数和等渗体积计算界面张力<sup>[45]</sup>。

当模拟压力大于地层油MMP时,CO<sub>2</sub>与原油形成多次接触混相,被混相带驱扫过的区域剩余油饱和度极低(图9)。

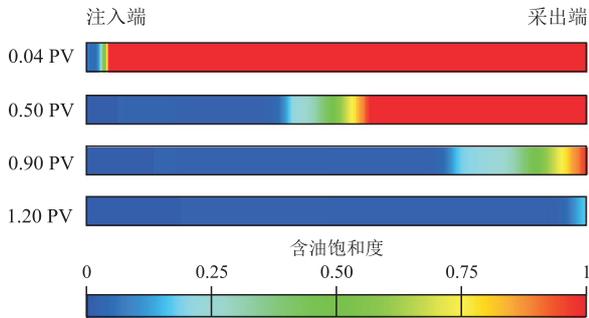


图9 不同注入量下含油饱和度分布

Fig.9 Oil saturation distribution with different injection pore volumes of CO<sub>2</sub>

结合图9和图10分析,可以观察到油气混合带,混合带前缘前端界面张力没有降低至 $10^{-3}$  mN/m,表明CO<sub>2</sub>与原油未形成一次接触混相。界面张力沿前缘前端向注入端逐渐减小,CO<sub>2</sub>与原油混合并抽提其中的轻组分后进入油气混合带的后缘,继续与新鲜的CO<sub>2</sub>进行传质;界面张力逐渐降低,当前缘前端到达第46个网格时界面张力降低至小于 $10^{-3}$  mN/m并趋近于0,最终形成具有一定宽度的混相带。混相带随着驱替的进行而缓慢向产出端推进,混相带宽度逐渐增大,并在细管模型出口端消失。

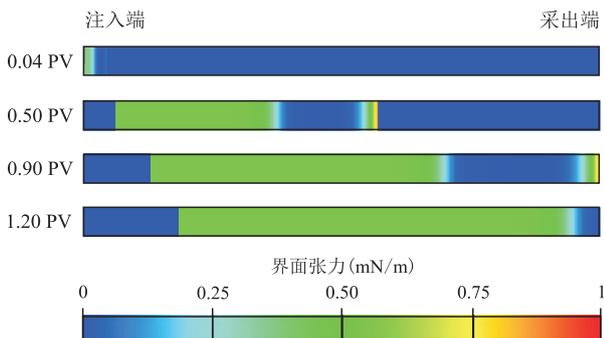


图10 不同注入量下界面张力分布

Fig.10 Interfacial tension distribution with different injection pore volumes of CO<sub>2</sub>

## 3 结论

不同油藏压力下MMP实验测试和数值模拟研究表明,当油藏压力低于原始饱和压力后,相应油样的CO<sub>2</sub>驱MMP呈小幅度递减的趋势。MMP的数值模拟计算值与实验值平均相对误差仅为0.43%,数值模拟模型的精度高。

随着油藏压力降低和溶解气脱出,各样品拟组分中,CH<sub>4</sub>摩尔含量降低幅度较大,C<sub>2</sub>和C<sub>3</sub><sup>+</sup>的摩尔含量变化较小,C<sub>7</sub><sup>+</sup>组分摩尔含量呈较大幅度的增加,C<sub>24</sub><sup>+</sup>组分摩尔含量增加幅度较为平缓;脱出气组分中,以CH<sub>4</sub>为主,只有当压力充分降低并趋于大气压时,C<sub>2</sub>和C<sub>3</sub><sup>+</sup>拟组分的摩尔含量才会大幅增加。

CO<sub>2</sub>与原油发生混相后,混相带出现在注入CO<sub>2</sub>波及前缘稍靠后的位置,混相带界面张力小于 $10^{-3}$  mN/m并迅速趋于0;混相带随着驱替过程的进行而向产出端移动,其宽度逐渐增大,并在模型出口端消失。

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编辑 单体珍